## PRINTER RUSH

(PTO ASSISTANCE)

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nozzles or slits and thereby the coagulation is achieved. The high pressures are produced by a so-called homogenizer. This technology does not work for elastomer dispersions due to clogging and jamming the equipment.

As suggested in DE ........ (filed of even date herewith, our reference number DYN 2000/U002) these difficulties can be overcome by generating high pressures with pressurized gases from 50 to 400 bar (5 · 10<sup>6</sup> to  $4 \cdot 10^7$  Pa).

In contrast to the process disclosed in US-A-5 463 021 the coagulation by this technique appears to be brought about by the rapid expansion of the dissolved gas, preferably via a nozzle.

The preferred gases for use with this process are nitrogen, air or  $CO_2$ .

In yet another coagulation process a volatile watermiscible organic solvent effects the coagulation. The
solvent is selected from the group consisting of alkanols of
1 to 4 carbon atoms and ketones of 2 or 3 carbon atoms. The
said solvents should not have a significant swelling effect
onto the said polymer, lest the coagulated or agglomerated
polymer becomes too sticky thus impairing the work-up.

Mechanical and thermal methods for coagulating polymers are known from US-A-5 463 021, EP-B-0 084 837,

EP-B-0 226 668 and EP-B-0 460 284.

After being coagulated the fluoropolymer may be dewatered. One method of dewatering the polymer is by mechanical dewatering. This process is described in US-A-4 132 845.

The wet polymers can be dried, usually in a temperature range of from 110 °C, preferably 150 °C, to 250 °C, in the presence of a carrier gas like air or nitrogen.

In the following preferred embodiments with the respect to fluoroelastomers are described in more detail:

> German Patent Application number 10004229.5, filed on February 1, 2000, these difficulties can be overcome

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